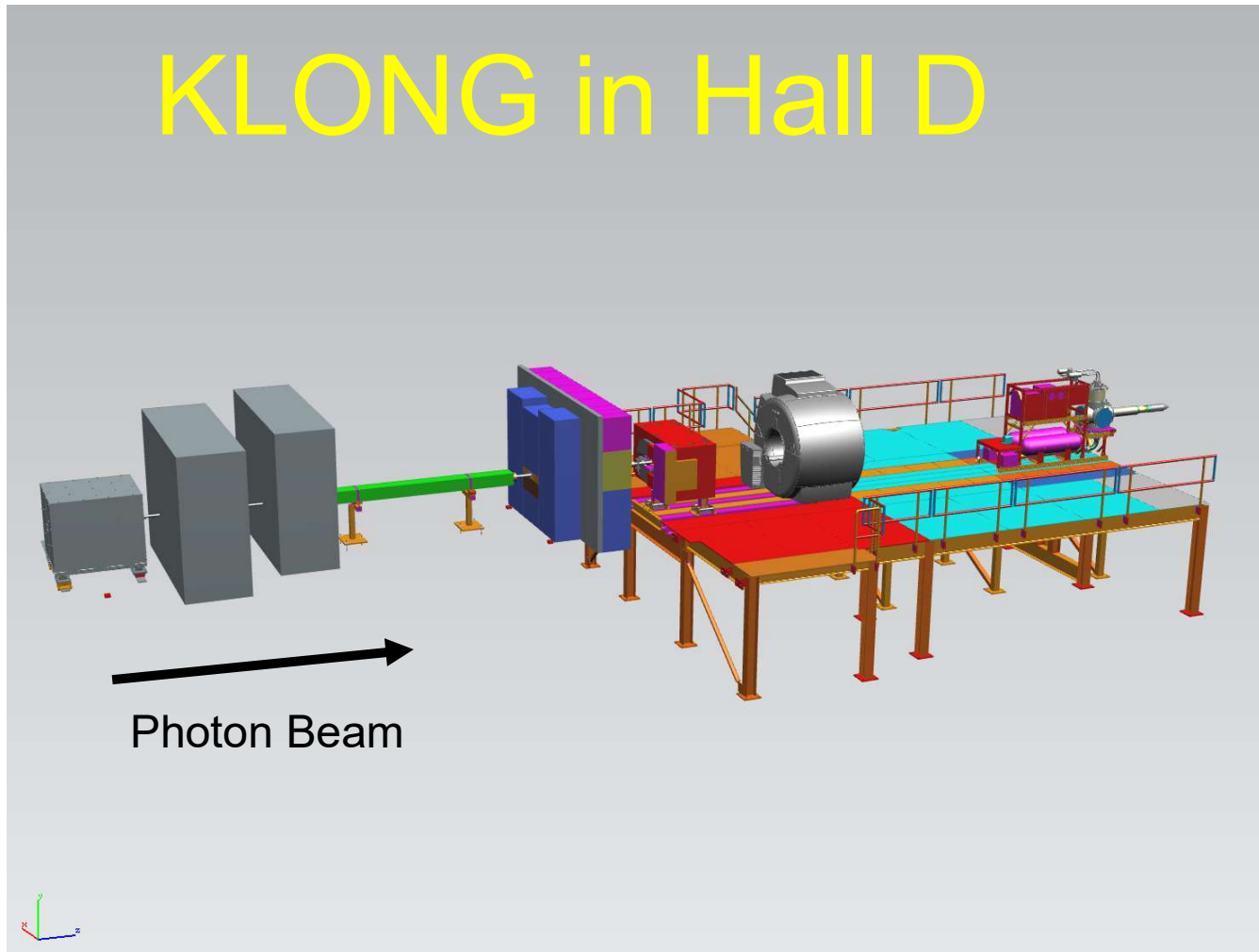
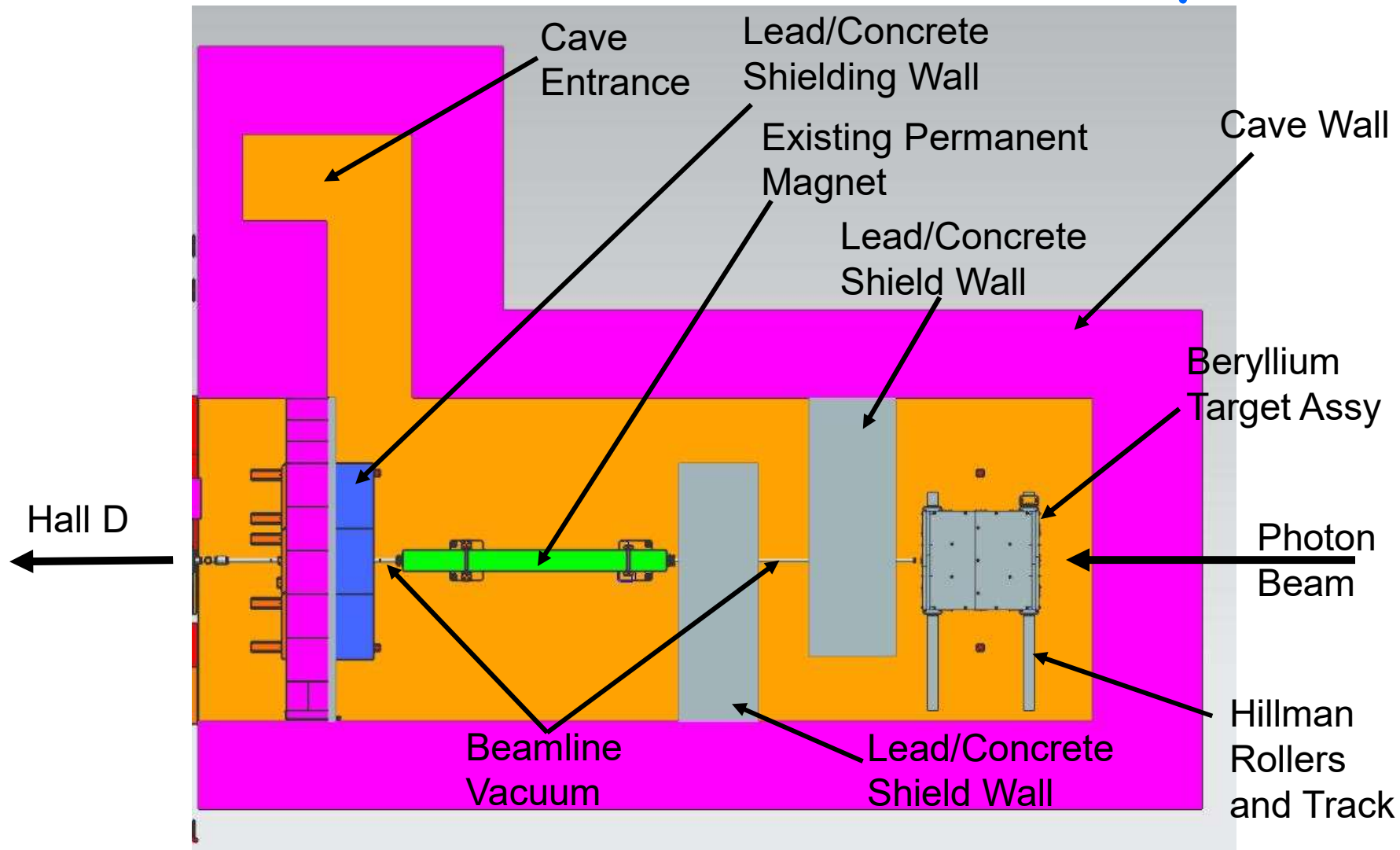


Engineering Update

KLONG in Hall D



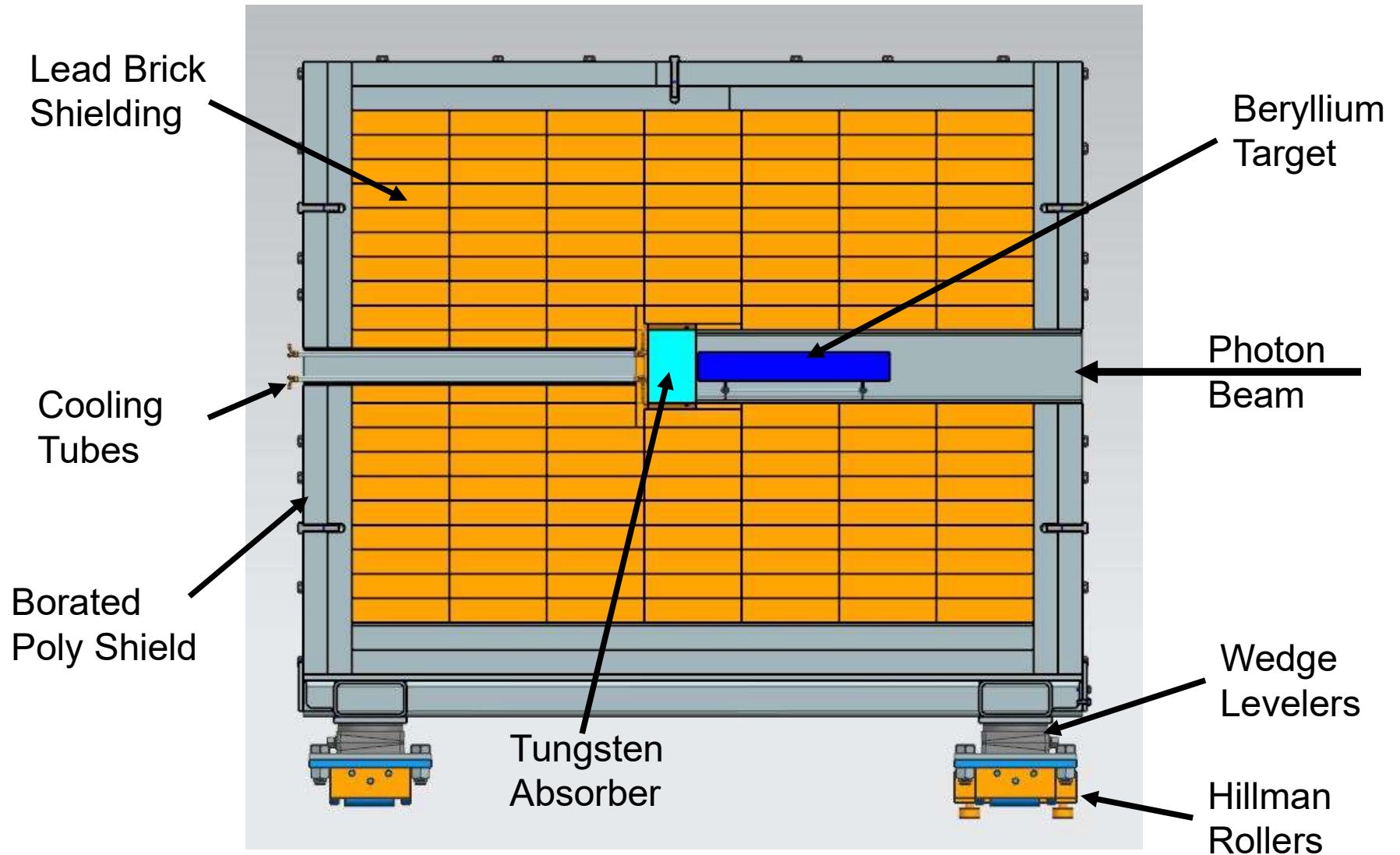
Hall D Collimator Cave Layout



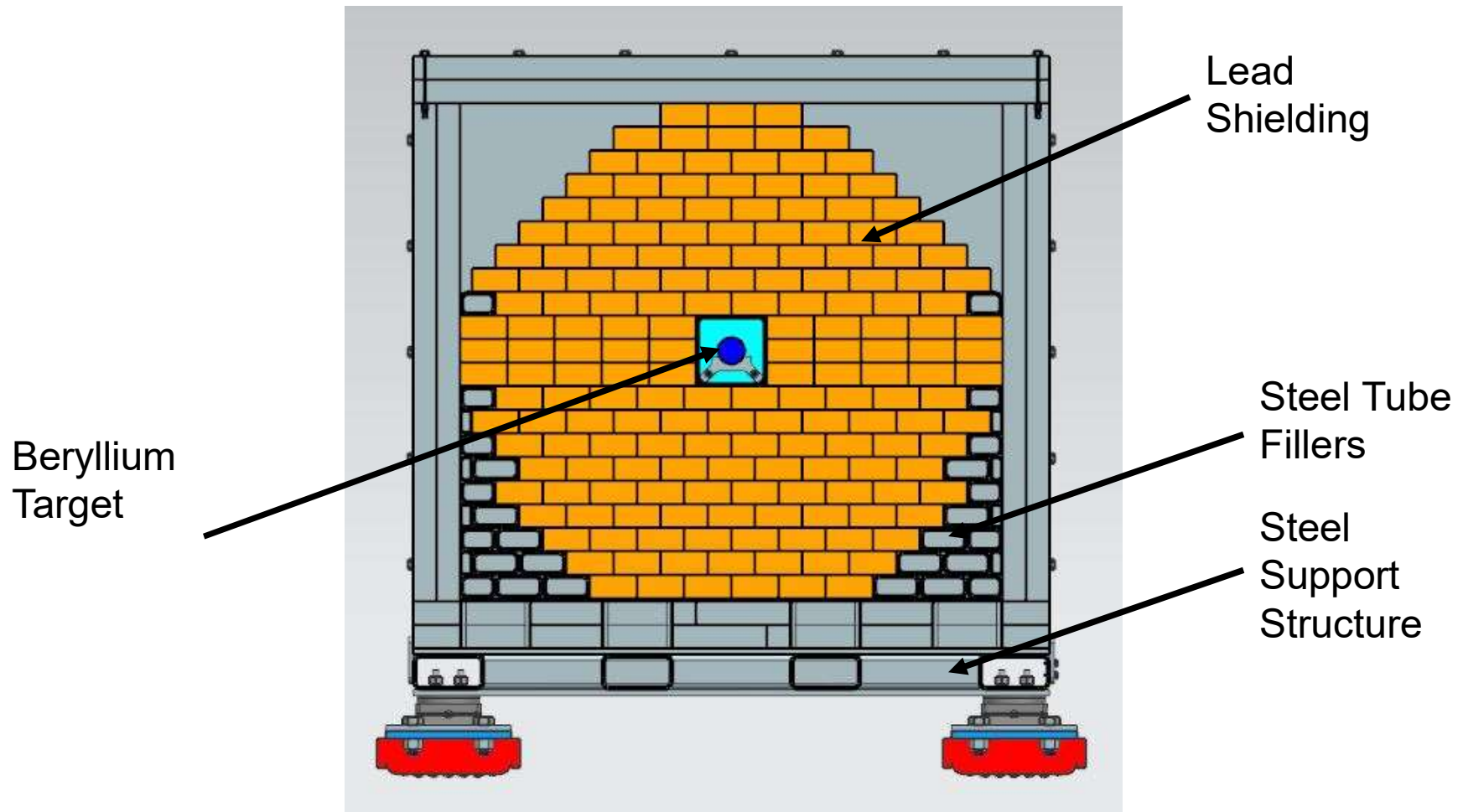
Cave Layout Elevation



Beryllium Target Assy



Beryllium Target Section



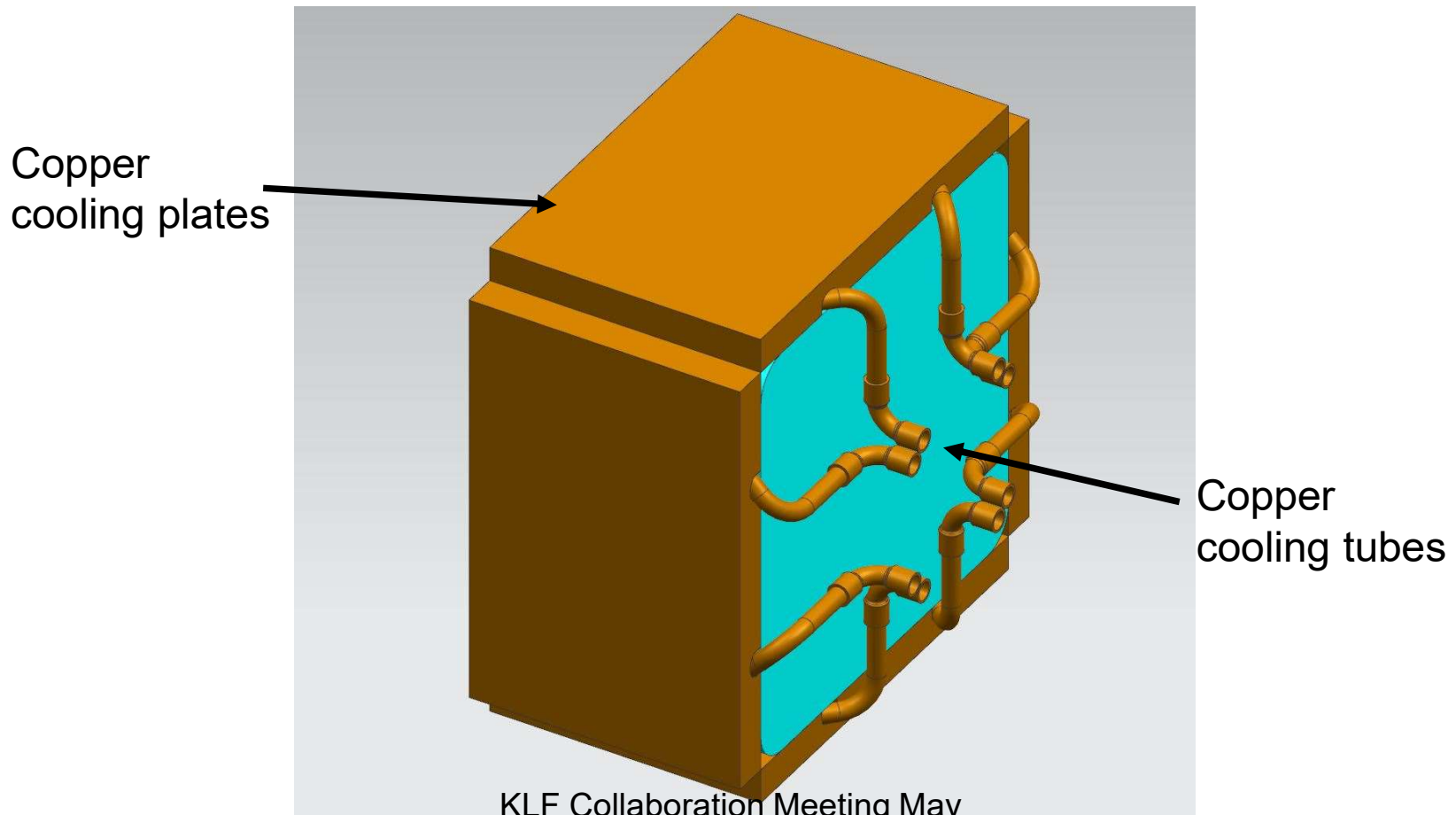
Design Requirements/Specs

- Beryllium Target
 - 6cm diameter
 - 40 cm length
 - 500W power absorption
 - Max Temperature 400C (factor of 3 to melting)
 - Air cooled
- Tungsten absorber
 - 15cm square
 - 10cm length
 - 5.2KW power absorption
 - Max Temperature inside 1000C (factor of 3 to melting)
 - Water cooled – separate LCW system required

Tungsten Absorber Thermal Analysis

- Power absorption data provided by Vitaly Baturin
- Modelled in ANSYS Static Thermal
- Shows maximum delta T of 216C
- Outer Surface cooled with water under 100C
- Maximum Tungsten Temp 316C

3D Rendering - cooling plates on 4 sides - Max water temp less than 100C



Cooling Water removing 6KW from Tungsten

KLong System cooling water - tanabe [Compatibility Mode] - Excel

File Home Insert Page Layout Formulas Data Review View Acrobat Tell me what you want to do... Timothy Whitlatch Share

L42

1 **KLong 6KW total, 2 circuits LCW**

2 Units Units Units Units

3 d 4.6 mm 0.015092 ft 0.0046 M ID of tube

4 L 10 m 10000 mm

5 epsilon 0.0000155 ft²/sec at 5°C 0.000005 ft e/d = 0.000331

6 Coil Power 3 kW 3000 W

8

9

10 $v = -2 \sqrt{\frac{2g\Delta P d}{0.433 L}} \log_{10} \left(\frac{\epsilon}{3.7d} + \frac{2.51}{v \sqrt{\frac{2g\Delta P d}{0.433 L}}} \right)$

11

12

13

14

15 $\frac{1}{\sqrt{f}} = -2 \log_{10} \left(\frac{\epsilon}{3.7d} + \frac{2.51}{v \sqrt{\frac{2g\Delta P d}{0.433 L}}} \right)$

16

17 $q = \frac{v \cdot d^2}{4} \cdot \rho \cdot \frac{gpm}{4}$

18 $Re = \frac{v d}{\nu}$

19 $\Delta T = \frac{3.8 P}{q}$

20 P=mCpDeltaT

21 3.8 factor= 1kg/s=15.83gpm

22 Cp = 4.18 KJ/Kg°C

23 KW=KJ/s=(kg/s)(kJ/kg°C)

24

25

26 DeltaP $\frac{2g\Delta P d}{0.433 L}$ f v Re q DT

27 (psi) (ft/sec) (no units) (ft/sec) (deg.C)

	V	DP	h
28	1.4	0.30948665	0.008419
29	2.8	0.43768022	0.005979
30	8	0.7398146	0.003574
31	20	1.16974958	0.002293
32	40	1.65427573	0.001648
33	45	1.75462438	0.001559
34	50	1.84953649	0.001483
35	55	1.93981023	0.001418
36	60	2.02606571	0.001362
37	65	2.10879605	0.001312
38	70	2.18840108	0.001268
39	75	2.26521033	0.001228
40	80	2.33949917	0.001191
41	85	2.41150054	0.001159
42	90	2.48141359	0.001128
43	95	2.54941011	0.001101
44	100	2.61563959	0.001075
45	105	2.680233	0.001051
46	110	2.74330594	0.001029
47	115	2.80496096	0.001009
48	120	2.86528961	0.000989
49	125	2.92437396	0.000971
50	130	2.98228798	0.000954
51	135	3.03909857	0.000938
52	140	3.09486649	0.000922
53	145	3.14964714	0.000908
54	150	3.20349117	0.000894

Heat Exchange with water at 70 psi DP

Twater = 37.59972858 C average

Nud = 65 From Oliver & Meyer paper for Re + 5000 81.07461 from Dittus below

K = 0.623 W/MK From White pg 650

Pr = 4.84 extrapolate from White appendix F

h = Nud K/D W/M² K

h = 8803.26087

q = hA(Tw-Twall) = mCpDeltaT = coil power

A = piDL use L for area inside cooling blocks, 2 per circuit L = 0.4 m

Twall = 96.55314416 C

Evaporation, Condensation and Heat Transfer

Fig. 7. Heat transfer results for the fully developed smooth tube

KW=KJ/s=(kg/s)(kJ/kg°C)

Forced convection in turbulent pipe flow

Gnielinski correlation

Gnielinski's correlation for turbulent flow in tubes [7]

$$Nu_D = \frac{(f/8)(Re_D - 1000)Pr}{1 + 12.7(f/8)^{1/2}(Pr^{2/3} - 1)}$$

where f is the Darcy friction factor that can either be obtained from the Moody chart or for smooth tube

$$f = (0.79 \ln(Re_D) - 1.64)^{-2}$$

The Gnielinski Correlation is valid for [7]

0.5 ≤ Pr ≤ 2000

3000 ≤ Re_D ≤ 5 × 10⁶

Dittus-Boelter equation

The Dittus-Boelter equation (for turbulent flow) is an explicit function for calculating the Nusselt number across the fluid. It is tailored to smooth tubes, so use for rough tubes (most commercial applications)

$$Nu_D = 0.023 Re_D^{4/5} Pr^n$$

where:

D is the inside diameter of the circular duct

Pr is the Prandtl number

n = 0.4 for the fluid being heated, and n = 0.3 for the fluid being cooled [8]

The Dittus-Boelter equation is valid for [11]

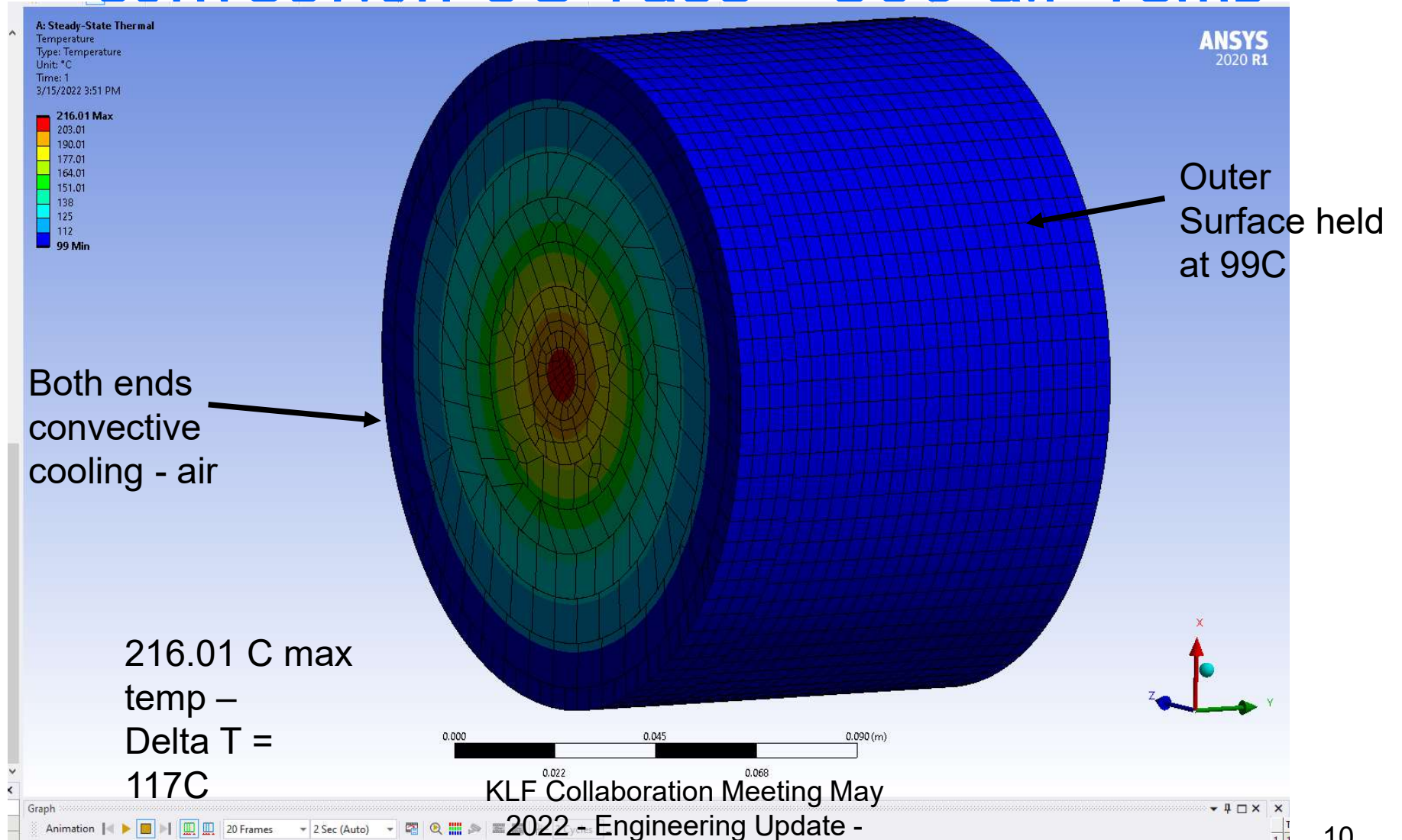
For L=40 m, d=3.5 mm.

For L=40 m, d=3.5 mm.

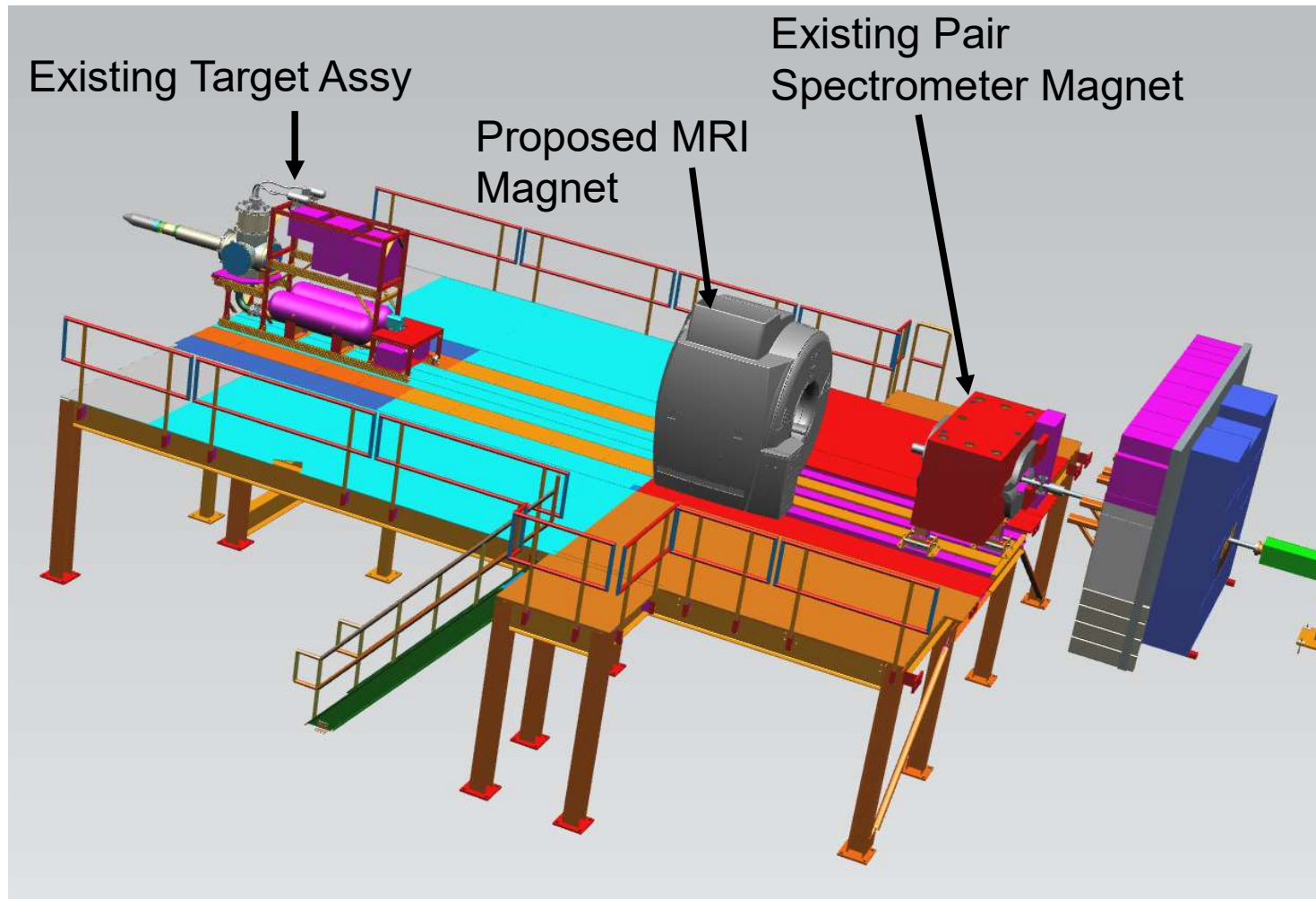
2 para circuits air-n2 Hx

Ready

5.2 KW total input - 2 W/m^2
convection US face - 80C air temp



Conceptual Setup in Hall D



Status

- Collimator Cave Preliminary Drawings 90% Complete
- Thermal Analysis needed on Beryllium
- Full Installation Plan Needed
- Beamline Requirements set
- Flux Monitor in Conceptual Phase – Proposed MRI will fit
- Separate meetings required for MRI Integration

Backup